



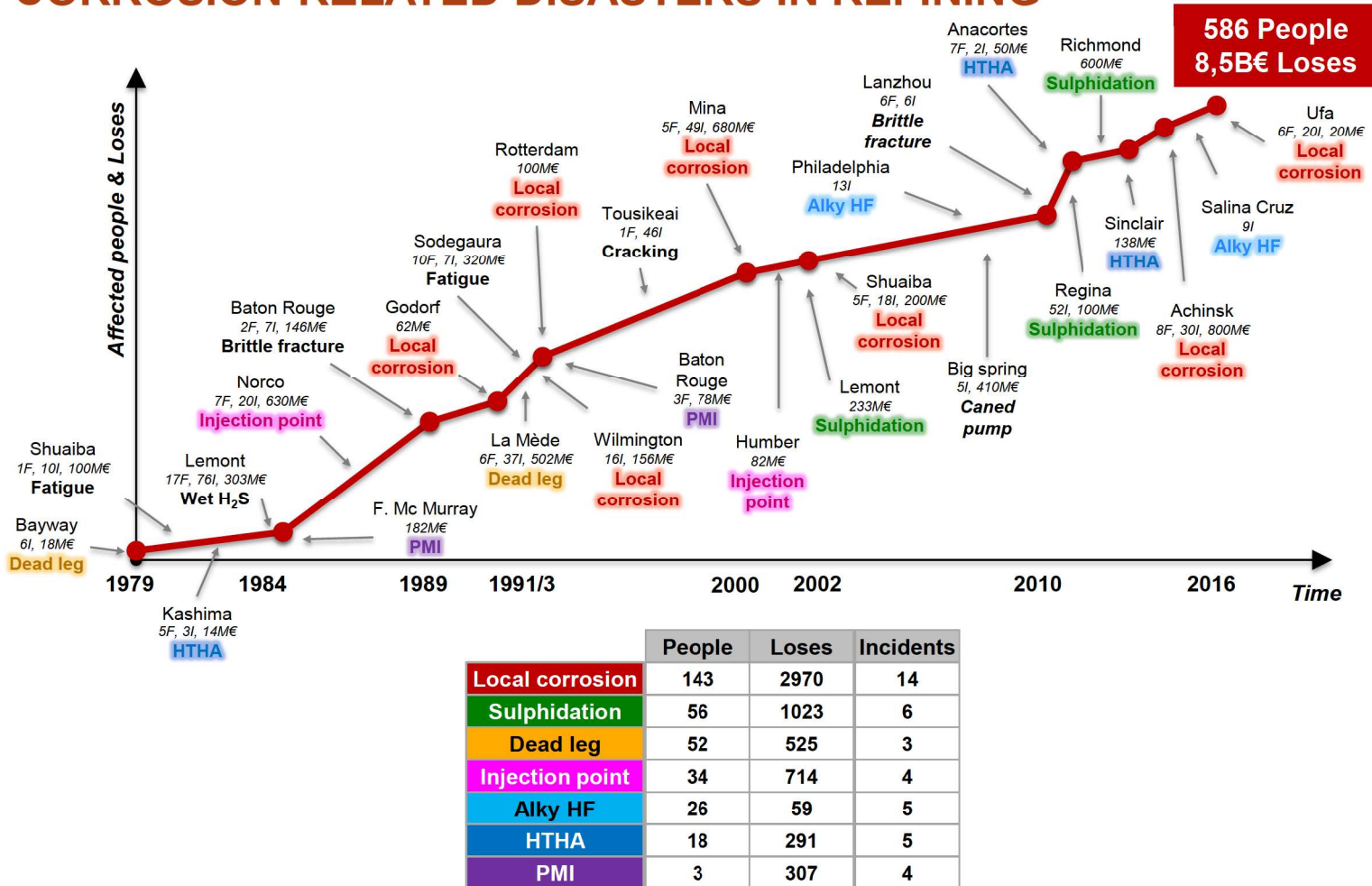
# **RISK-BASED INSPECTION METHODOLOGY**

## **API Recommended Practice 580/581**

EPERC Seminar Rome, April 1<sup>st</sup> to 3<sup>rd</sup> of 2019

Ricardo Gonzalez, TOTAL Refining & Chemicals

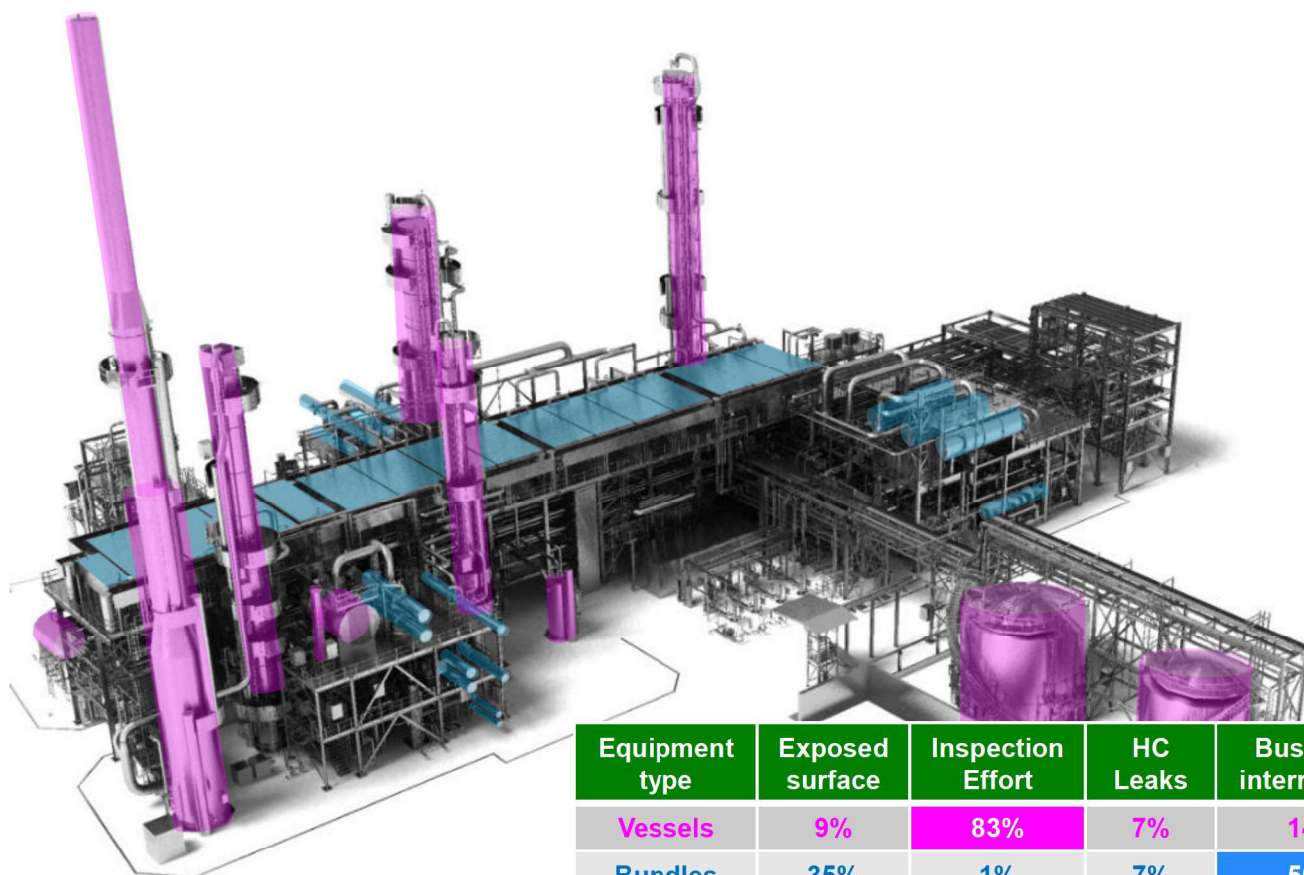
# CORROSION-RELATED DISASTERS IN REFINING



## THE DIFFERENT INSPECTION APPROACHES

	Approach based on...			Risk based
	Reactive inspection	Calendar	Condition	
Strategy	Run to Failure	Focus on regulations	Equipment life	Risk management
Scope	Critical equipment	Everything... you are aware!	Unit cycle limiting equipment	Whatever is needed to operate at acceptable risk
Benefits	Reduced budget	Levelled scope	Run length assurance	Reduced risk & scope, improved availability
Issues	Costly failures, uncertainty	Increased budget, costly failures	Costly decisions	Cultural change

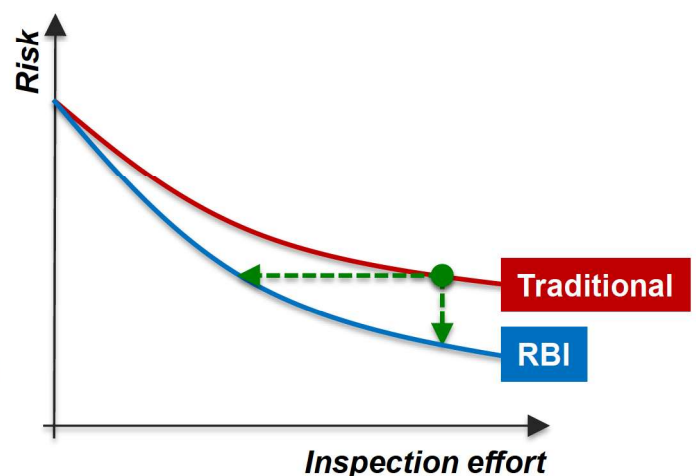
## REFINING INSPECTION BACKGROUND



Equipment type	Exposed surface	Inspection Effort	HC Leaks	Business interruption
Vessels	9%	83%	7%	14%
Bundles	35%	1%	7%	50%
Piping	56%	16%	78%	32%

## API RISK-BASED INSPECTION (API RBI)

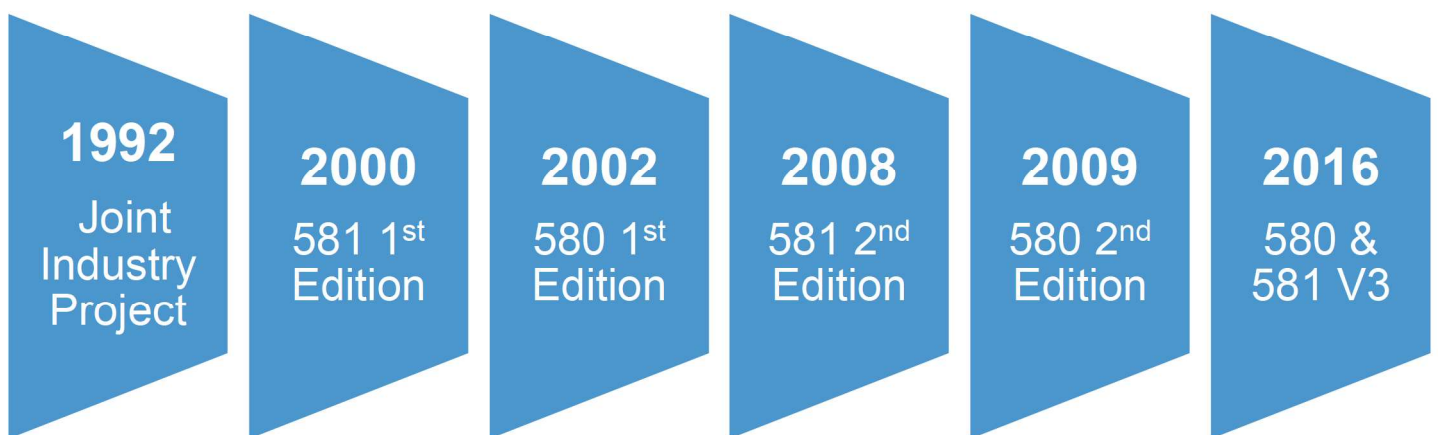
- This methodology may be used to **manage the overall risk of a plant** by focusing inspection effort on the high risk equipment
- It provides the basis for **making informed decisions** on inspection scope, frequency, and the suitable NDT
- In most processing plants, a large percent of the total unit **risk will be concentrated in a relatively small percent** of equipment items
- These potential **high-risk** components may require **greater attention**, through a revised inspection plan
- The cost of increased inspection effort may be **offset by reducing excessive inspections** in the areas having lower risk



NDT: Non destructive testing



## API RBI HISTORY & DOCUMENTS



- Document 580 introduced the principles and present **minimum general guidelines for RBI**
- Document 581 provides **quantitative RBI methods** for inspection planning

## DOCUMENT 580

### ➤ Content

- What is RBI and its key elements
- How to implement and sustain it

### ➤ Purpose: *Using RBI as **continuous improvement tool***

- Refresh view when changes occur
- Identify other risk mitigation opportunities
- Promotes deployment of new technology

### ➤ Scope: *Target audience*

- Primarily inspection
- Requiring **involvement from Engineering Maintenance and Operations**

### ➤ Reassessment: *Reasons and when to conduct*

- Damage progression & inspections
- Effect of **mitigation strategies**
- Following process or physical changes
- After Maintenance Turnarounds

## DOCUMENT 581

- Provides quantitative procedures to establish an inspection program using RBI methods for pressurized fixed equipment
- Risk calculation
  - Determination of probability combined with consequence of a failure (POF, COF)
  - Failure: loss of containment from pressure boundary
  - Risk increases as damage accumulates during in-service operation
  - As risk tolerance is approached, sufficient inspection effectiveness is required to quantify damage state
- Risk management
  - On-site risk to employees
  - Off-site risk to the community
  - Business interruption risks
  - Risk of damage to the environment

## Document organization

**Part 1:** Inspection Planning

**Part 2:** Determination of probability of failure

**Part 3:** Consequence modeling

*POF: Probability of failure, COF: Consequence of failure*



## RISK ANALYSIS

- In general, risk is calculated as function of time as follows

$$R(t) = POF(t) \cdot C(t)$$

- The probability of failure is a function of time, since damage due to cracking, thinning or other damage mechanism increases with time
- In API RBI, the consequence of failure is assumed to be independent of time, therefore

$$R(t) = POF(t) \cdot CA \quad \text{for Area-based Risk}$$

$$R(t) = POF(t) \cdot FC \quad \text{for Financial-based Risk}$$

*POF: Probability of Failure*

## TARGETS

- Defined as the maximum level acceptable for continued operation to trigger an inspection or other mitigation such as:
- **Risk target:** A level of acceptable risk (e.g. an area of 3,25 m<sup>2</sup>/yr.)
  - **POF Target:** A frequency of failure or leak per year that is considered unacceptable (e.g. 3,06E04)
  - **Damage Factor (DF) Target:** A damage state that reflects an unacceptable failure frequency factor greater than the generic (e.g. 1000)
  - **COF Target:** A level of unacceptable consequence in terms of Area or Financial<sup>(\*)</sup>
  - **Thickness Target:** A specific thickness (e.g. minimum required thickness  $T_{min}$ )
  - **Maximum interval Target:** Specific inspection frequency considered unacceptable (e.g. 15 yrs.)

*(\*) As COF can't be reduced through inspection, mitigation should be reducing inventory or ignition*

## PROBABILITY OF FAILURE (1/4)

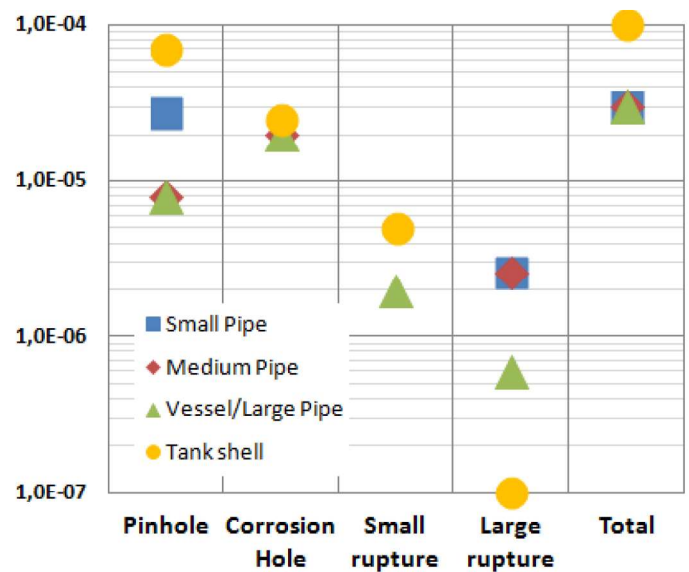
- The probability of failure in API RBI is determined by three parameters:
- *Generic failure frequency*
  - *Damage factor*
  - *Management system factor*

$$POF(t) = gff \cdot D_f \cdot F_{MS}$$

Based on industry data


- ✓ *Due to fabrication flaws*
- ✓ *Non-service related damage*
- ✓ *Prior to operating exposure*







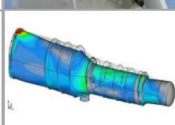
Generic failure frequency



## PROBABILITY OF FAILURE (2/4)

- The damage factor is the amount of damage as a function of time and the effectiveness of inspection

$$POF(t) = gff \cdot \boxed{D_f} \cdot F_{MS}$$


$D_f^{thin}$		Internal corrosion
$D_f^{elin}$		Lining damage
$D_f^{extd}$		External corrosion
$D_f^{scc}$		Stress corrosion cracking
$D_f^{htha}$		High temperature H <sub>2</sub> Attack
$D_f^{brit}$		Brittle fracture
$D_f^{mfat}$		Mechanical fatigue

$$D_{f-total} = \min [ D_f^{thin}, D_f^{elin} ] + D_f^{extd} + D_f^{scc} + D_f^{htha} + D_f^{brit} + D_f^{mfat}$$

## PROBABILITY OF FAILURE (3/4)

➤ Example of internal corrosion<sup>(\*)</sup>. Main parameter is aging factor  $ar/t$

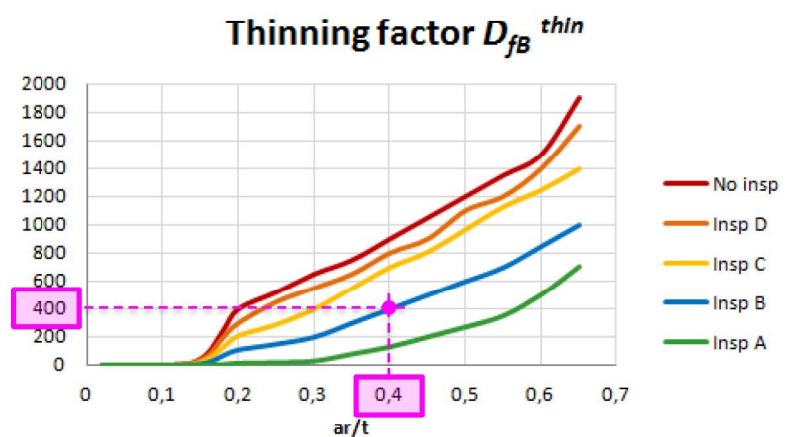
- $a$ : Time (e.g. 20 yrs.)
- $r$ : Corrosion rate (e.g. 0,21 mm/yr.)
- $t$ : Thickness (e.g. 10,5 mm)

$$ar/t = 20 \cdot 0,21 / 10,5 = 0,4$$

### Using formula of API 581 V2

For 20 years & 1 Inspection B in the history

$$D_f^{thin} = D_{fB}^{thin} (400) / F_{OM(**)}(10) = 40$$




(\*) Using API 581 V2 model (V3 introduces a more complex model for thinning), (\*\*) Monitoring of main process variables



## PROBABILITY OF FAILURE (4/4)

- Based on the result of an Audit protocol, it accounts for the influence of the facility's management system in place (PSM, MOC, Mechanical integrity, etc.)
- Assumes that the chance of identifying accumulated damage during inspection is proportional to the quality of PSM program

$$POF(t) = gff \cdot D_f \cdot F_{MS}$$


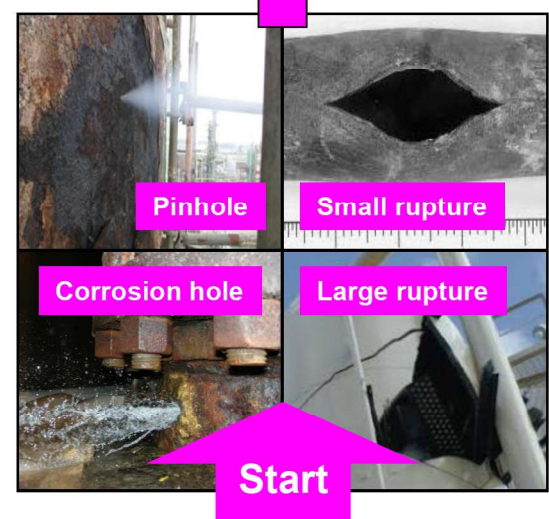
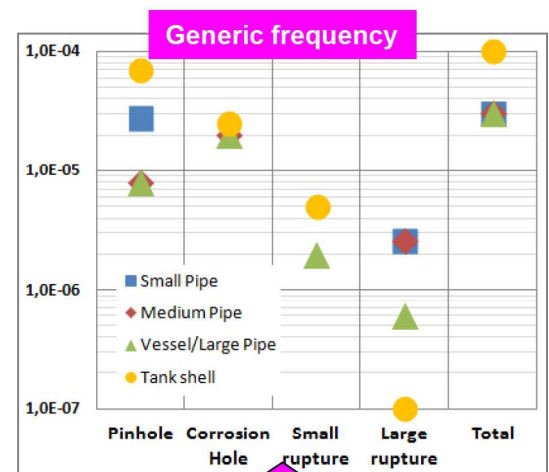
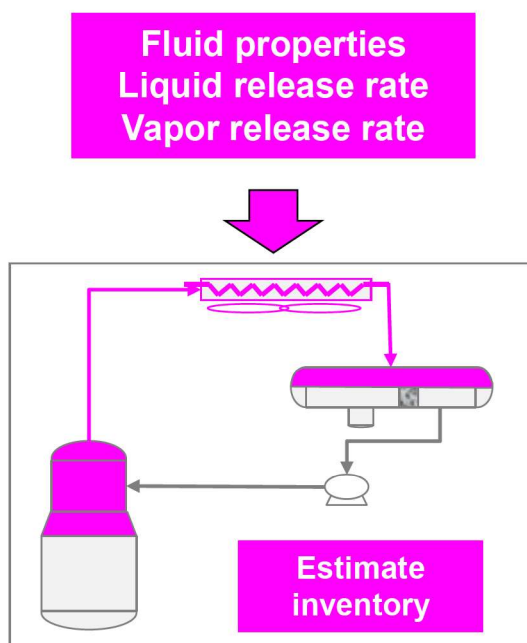
- ✓  $F_{MS} = 10^{(-0,02 \cdot Pscore + 1)}$
- ✓ *Pscore as percent of the audit result*
- ✓ *Frequently set to 0,4 in the industry*

Title	Questions	Points
Leadership	6	70
Process safety information	10	80
Process Hazard Analysis	9	10
MOC	6	80
Operating procedures	7	80
Safe work practices	7	85
Training	8	100
Mechanical integrity	20	120
Pre-startup safety review	5	60
Emergency response	6	65
Incident investigation	9	75
Contractors	5	45
Audits	4	40
<b>Total</b>	<b>101</b>	<b>1000</b>

**PSM:** Process safety Management, **MOC:** Management of Change

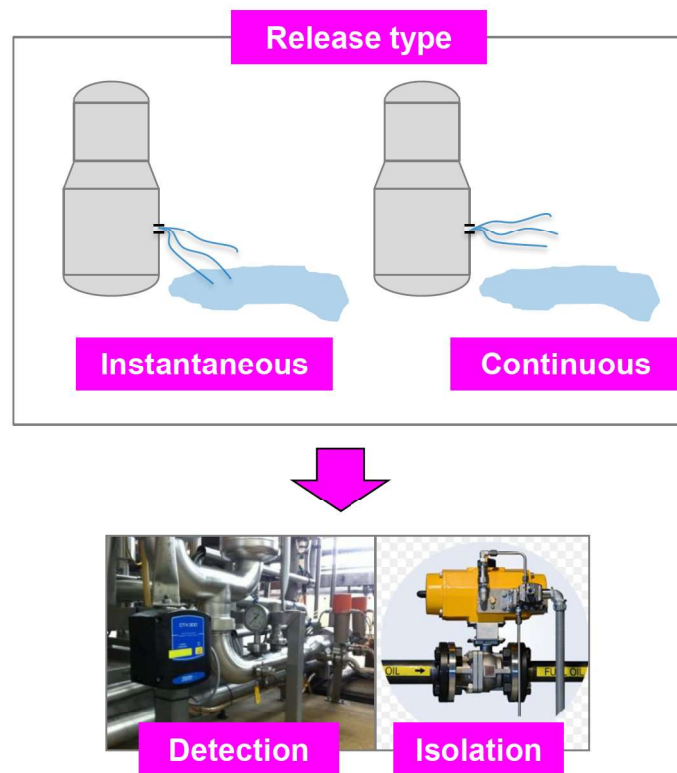
## CONSEQUENCE OF FAILURE (1/4)

- Select hole sizes, Determine fluid properties, calculates release rate and estimate fluid inventory



## CONSEQUENCE OF FAILURE (2/4)

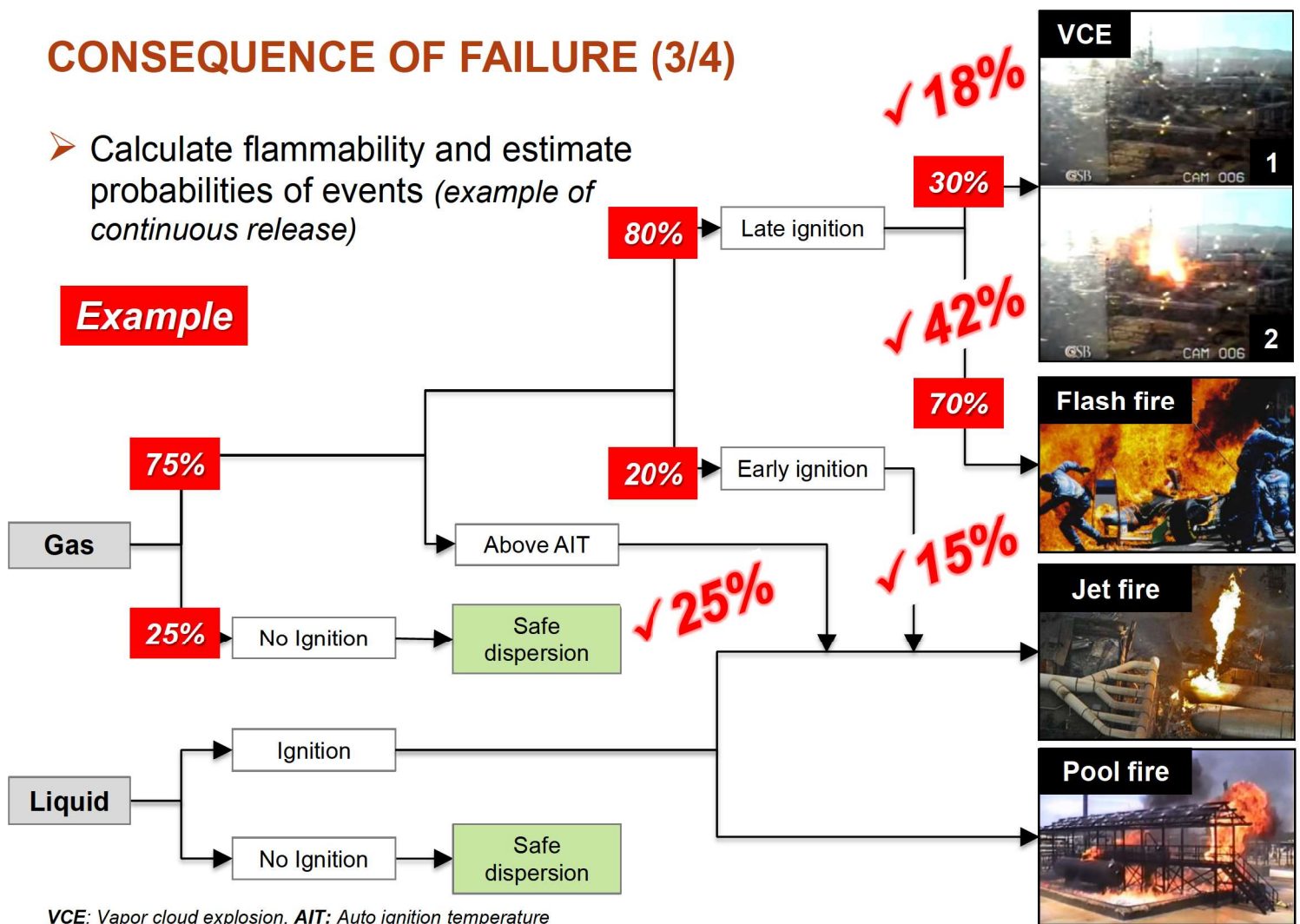
- Determine release type and assess detection and isolation systems



## CONSEQUENCE OF FAILURE (3/4)

- Calculate flammability and estimate probabilities of events (example of continuous release)

### Example



VCE: Vapor cloud explosion, AIT: Auto ignition temperature

## CONSEQUENCE OF FAILURE (4/4)

### ➤ Calculation of toxic consequence

- *Common chemical industry toxic materials & representative fluid*
- *Determination of toxic release and probabilities*
- *Toxic COF for HF, H<sub>2</sub>S, Ammonia and Chlorine*

### ➤ Non-Flammable Non-Toxic consequences

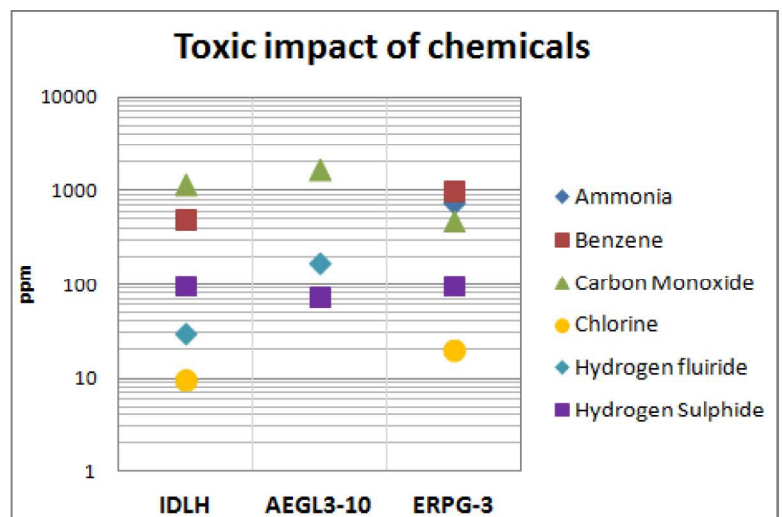
- *Steam, acid caustic leaks*

### ➤ Environmental consequence

- *Based on remediation & clean-up cost*

### ➤ Financial consequence

- *Cost of equipment (and surroundings) repair and replacement*
- *Business interruption*

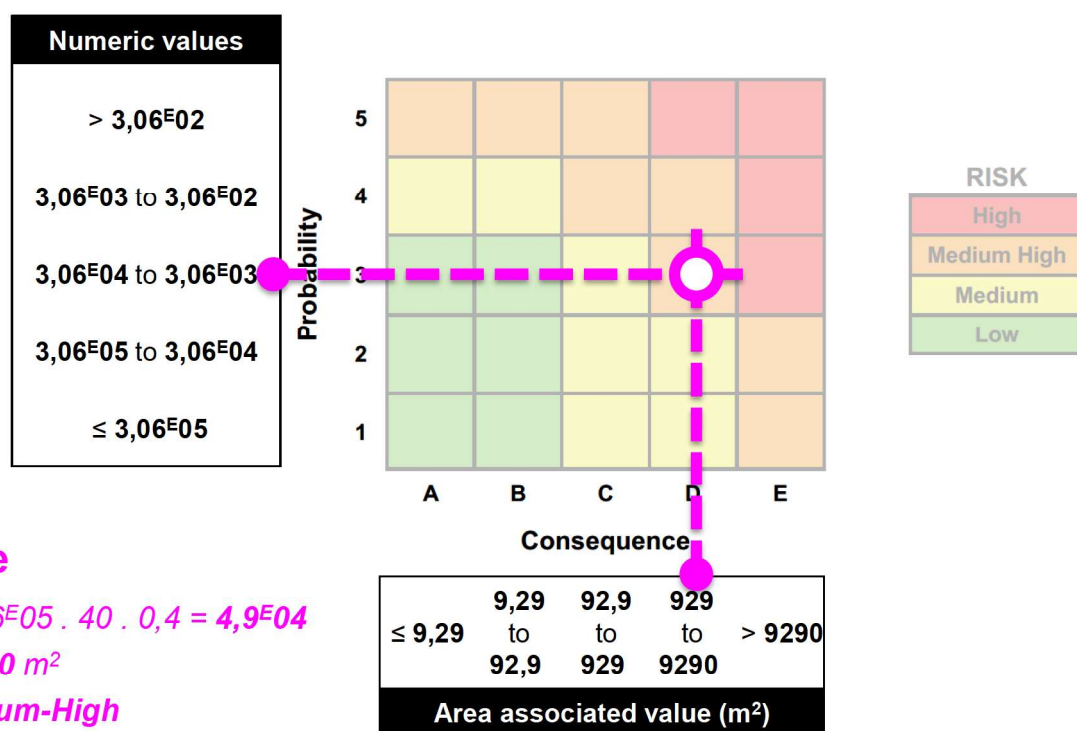


*IDLH: Immediately dangerous to life or health, AEGL3-10: Acute exposure guideline Level (10<sup>th</sup>), ERPG-3: Emergency response planification guideline*



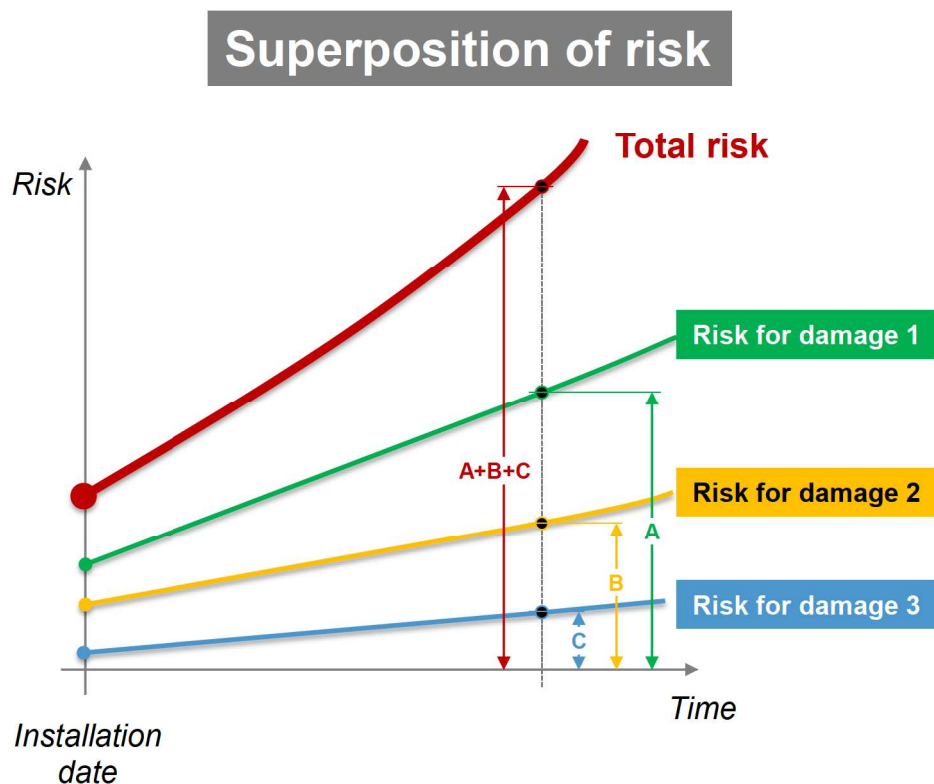
## FINAL RISK ANALYSIS

- Once the Probability and the maximum consequence are calculated, the result can be placed into the Risk Matrix



## INSPECTION PLANNING (1/5)

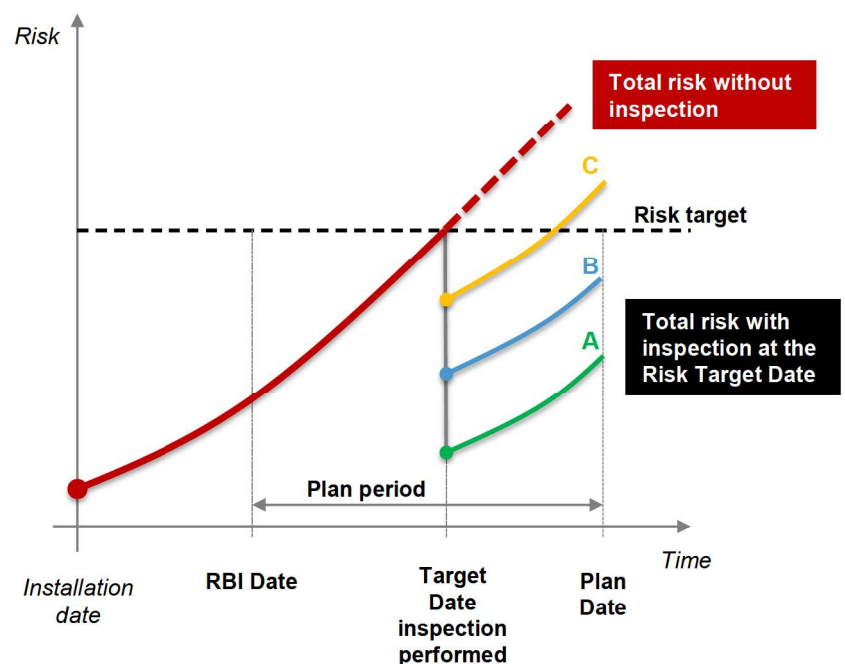
- Risk increases with time as component damage increases
- If multiple damage occurs at the same time, the principle of superposition is used to derive total risk
- At some point in time, risk reaches the user's specified risk target



## INSPECTION PLANNING (2/5)

- Inspection planning involves recommending the number and level of inspection required to reduce risk to acceptable value at plan date
- Inspection effectiveness is graded A to E with A providing the greatest certainty of finding damage and E representing no inspection

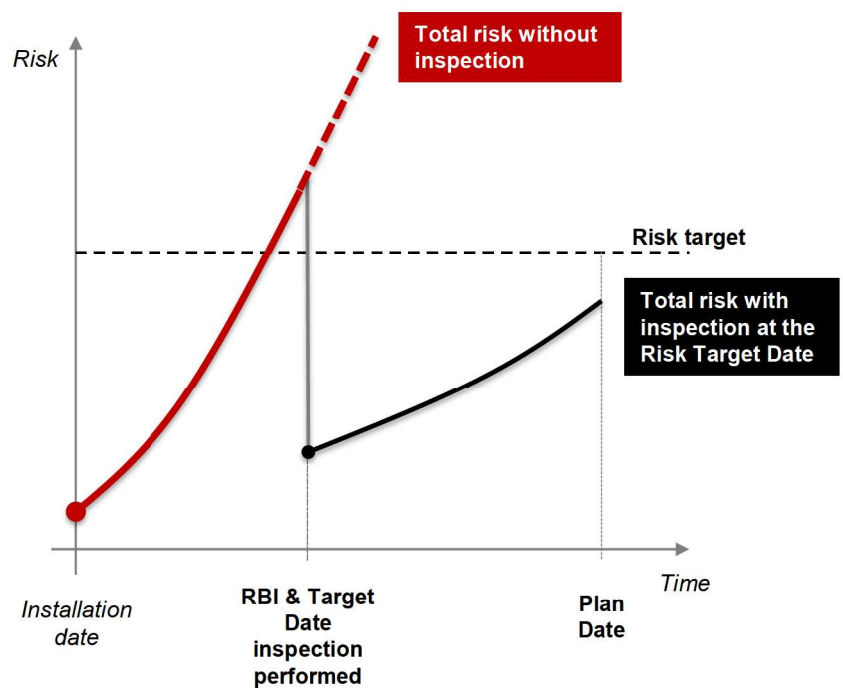
### Case 1: Risk exceeding target between RBI Date and Plan date



## INSPECTION PLANNING (3/5)

- For many applications, the user's risk target has been exceeded at the time of the RBI analysis is performed
- Inspection is recommended immediately

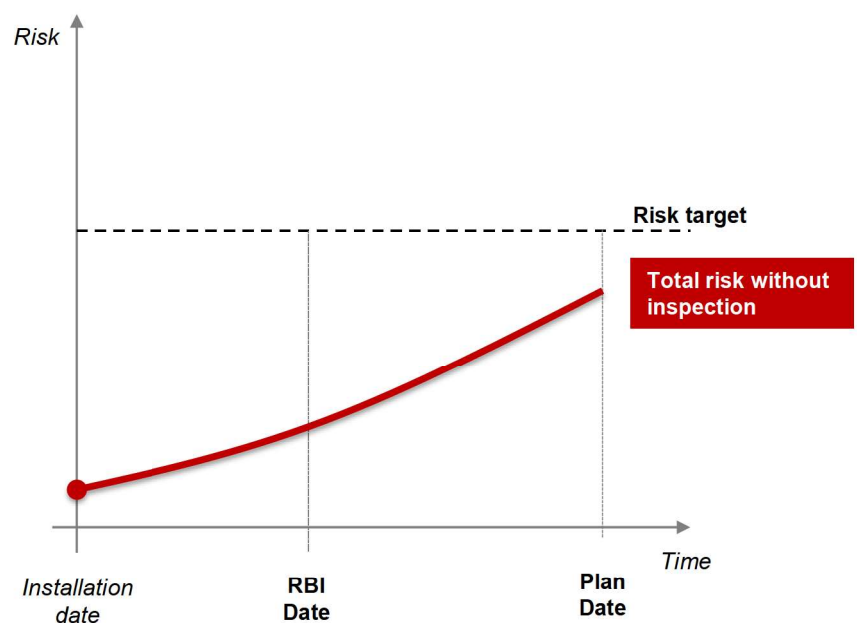
### Case 2: Risk exceeding target prior to the RBI Date



## INSPECTION PLANNING (4/5)

### Case 3: Risk not exceeded prior to the Plan Date

- When the risk is determined to be acceptable at the plan date, inspection is not required





## INSPECTION PLANNING (5/5)

- The inspection plan is developed based on the three previous cases
- Equipment is modeled as a group of individual components in API RBI
- The final inspection plan for the equipment is based on the results derived for the components
- The inspection plan includes:
  - Date of the required inspection
  - The type of NDT (e.g. Visual, UT, Radiography, WFMT) based on the active damage mechanism
  - The extent of inspection (e.g. percent of total area examined or specific locations)
  - Location of inspection (external or internal)

*UT: Ultrasonic testing, WFMT: Wet fluorescent Magnetic test*

## SUMMARY

- As technology and process optimization advances, the context for mechanical integrity in the industry becomes more complex every day
- Other disciplines are starting to follow the rules of quantitative risk-based for their decision-making process
- Inspection team need to produce a step change to become stakeholder in mechanical integrity assurance through risk management
- Quantitative RBI as per API 581 settles the basis for sound risk management of installations

## REFERENCES

- API 580 Recommended practice version 2016
- API 581 Recommended practice version 2008 & 2016
- Industry Statistics, TOTAL RC Industrial Division
- Risk-based inspection reassessment, RBI Summit 2009, The Equity Engineering Group





# BACKUP

## EXAMPLE 2 NEW THINNING MODEL OF API 581

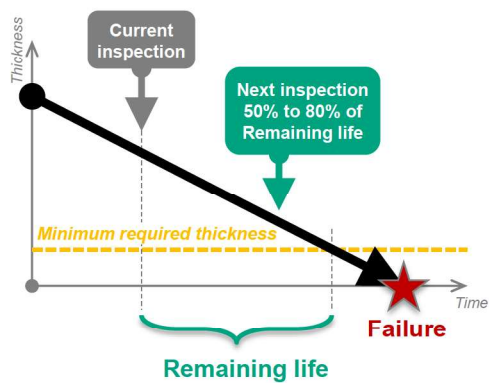
- Version 3 of document released in 2018 contains a new model for assessing POF related to metal loss.
- In general terms this model includes:
  - Determination of furnished thickness, corrosion rate, effectiveness of past inspection and time in service
  - Determination of minimum required thickness through FFS or code calculation
  - Calculate  $ar/t$  factor including clad (if exist)
  - Calculate strength ratio using flow stress and the average of tensile & yield stress of the material
  - Calculate the inspection effectiveness factor and the posterior probability depending on those factors (Bayesian approach)
  - Determine the damage factor using affecting the previous calculated parameters by a standard normal cumulative distribution function
  - Affect the calculated damage factor by the on-line monitoring, dead-legs, etc. as in version 2.

*FFS: Fitness-for-service,  $ar/t$ : Aging factor (Period.Corrosion rate / Thickness)*

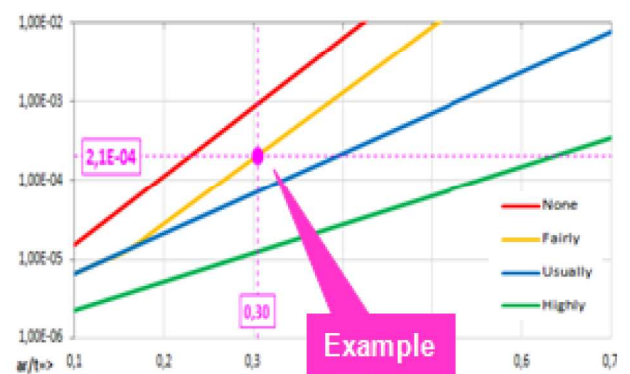


## RBI – MAIN CHANGE

### REMAINING LIFE



### RBI



PROBABILITY	>9E-03	9E-03	9E-04	9E-05	9E-06
CONSEQUENCE					
	<200K€	200K€ to 2M€	2M€ to 10M€	10M€ to 100M€	>100M€

Not acceptable risk

Acceptable risk